Critical Densities of Pure Fluids from an Intersection Method Assuming Three-Dimensional Ising-like Systems:

Application to Refrigerants R32, R124, and R152a

(For Fluid Phase Equilibria)

Lambert J. Van Poolen

Engineering Department Calvin College 3201 Burton St. SE Grand Rapids, MI 49546

**KEYWORDS**: critical state; vapour-liquid equilibria; pure; refrigerant R32; refrigerant

R124; refrigerant R152a

**ABSTRACT** 

Liquid-vapor coexisting density and temperature data within 3 to 20 K of the critical point

at approximately 1 K intervals and critical temperatures obtained in earlier work are used to

test a novel method to estimate the critical density (p<sub>c</sub>) for refrigerants R32, R124, and

R152a. The critical density is determined by the intersection, at the critical temperature, of

the rectilinear diameter with a function based on maxima in the liquid volume fraction.

Functional forms are based on fluids modeled as three dimensional Ising-like systems. For

the determination of  $\rho_c$ , coexisting densities, temperatures, and the critical temperature are

allowed to vary as normally distributed variables about a mean (reported value) with a

standard deviation equal to one-third the reported uncertainty. Equally probable data

subsets are chosen randomly from the complete data set. Consistent results for  $\rho_{\text{c}}$  and its

uncertainty are achieved when the data selection - data fitting procedure is repeated one to

two hundred times. Critical densities agree with those in the literature within estimated uncertainties. Uncertainties at a  $2\sigma$  level for the critical temperatures used and for the critical densities obtained are on the order of 0.3 K and 1.0 kg/m<sup>3</sup>, respectively.

#### INTRODUCTION

Alternative refrigerants such as R32, R124, and R152a, are important as replacements for ozone depleting refrigerants. Knowledge of their coexistence and critical properties is necessary to design new systems using these alternative refrigerants. In this work, we utilize previously obtained critical temperatures and their uncertainties (Van Poolen *et al.* [1]) to test a novel method of obtaining critical densities - the intersection at the critical temperature of the rectilinear diameter and a function based on maxima in the liquid volume fraction ( $X_{(v)}$ ). The form of these functions is based on three dimensional Ising-like fluid models.

The saturated liquid density ( $\rho^{\ell}$ ), saturated vapor density ( $\rho^{v}$ ), and temperature (T) data and their respective uncertainties are given for R32 and R152a by Holcomb *et al.* [2] and for R124 by Niesen *et al.* [3]. Of these data, twelve points in the range of 338.24 to 348.61 K for R32, fourteen points in the range of 375.27 to 390.65 K for R124, and thirteen points in the range of 372.35 to 383.71 K for R152a are utilized along with previously obtained critical temperatures to estimate critical densities. The range of temperatures in the data sets is from 3 to 20 K below the critical point temperature. All temperatures are referenced to the ITS-90 temperature scale.

#### **PROCEDURE**

The following (truncated) expressions for the coexistence densities based on three dimensional Ising-like fluid systems (see Kiselev and Sengers [4]):

$$\rho^{\ell} = G_1 + G_2 \epsilon^{\beta} + G_3 \epsilon^{\beta + \Delta_1} + G_4 \epsilon^{\beta + 2\Delta_1}, \tag{1}$$

and,

$$\rho^{\nu} = G_1 - G_2 \epsilon^{\beta} + G_5 \epsilon^{\beta + \Delta_1} + G_6 \epsilon^{\beta + 2\Delta_1}, \tag{2}$$

where  $\epsilon=(T_c-T)/T_c$ , ( $\beta=0.325$  and  $\Delta_1=0.51$ , Kiselev and Sengers [4]), and  $G_1$  (an estimate for  $\rho_c$ ) -  $G_6$  are fitted constants, are the basis for the functional forms that follow. The difference in the coexistence densities is:

$$\rho^{\ell} - \rho^{\nu} = 2G_{2} \epsilon^{\beta} + (G_{3} - G_{5}) \epsilon^{\beta + \Delta_{1}} + (G_{4} - G_{6}) \epsilon^{\beta + 2\Delta_{1}}.$$
 (3)

The rectilinear diameter based on Eqs.(1) and (2) is given as:

$$\frac{\rho^{\ell} + \rho^{\nu}}{2} = G_7 + G_8 \epsilon^{\beta + \Delta_1} + G_9 \epsilon^{\beta + 2\Delta_1}, \tag{4}$$

where  $G_{7}$  (estimated  $\rho_{c}$  reported here) -  $G_{9}$  are separately fitted constants.

The functional form based on maxima in the liquid volume fraction is now developed (see Van Poolen [5]). The liquid volume fraction is:

$$X_{\ell\nu} = \frac{(\rho_t - \rho^{\nu})}{(\rho^{\ell} - \rho^{\nu})},\tag{5}$$

where  $\rho_t$  is the total or overall density. For constant values of  $\rho_t < \rho_c$ ,  $X_{\ell\nu}$  goes through a maximum as temperature varies. The appropriate derivative is:

$$\frac{\partial X_{\ell \nu}}{\partial \epsilon} \bigg|_{\rho_{t}} = \frac{(\rho^{\ell} - \rho^{\nu})(-\frac{d\rho^{\nu}}{d\epsilon}) - (\rho_{t} - \rho^{\nu})(\frac{d\rho^{\ell}}{d\epsilon} - \frac{d\rho^{\nu}}{d\epsilon})}{(\rho^{\ell} - \rho^{\nu})^{2}}, \tag{6}$$

and  $\rho_x$  (  $\rho_t$  for which this derivative is zero (for  $T < T_c$ ), is:

$$\rho_{x} = \rho^{v} + \frac{(\rho^{\ell} - \rho^{v})}{1 - \left[\frac{d\rho^{\ell}}{d\epsilon} / \frac{d\rho^{v}}{d\epsilon}\right]}.$$
(7)

In the limit  $T \rightarrow T_c$ , the ratio of derivatives goes to -1 and all the densities go to  $\rho_c$ , hence,  $\rho_x \rightarrow \rho_c$ . Substituting Eqs. (1) and (2) and their derivatives into Eq. (7) yields:

$$\rho_{x} = G_{7} + G_{10} \epsilon^{\beta + \Delta_{1}} + G_{11} \epsilon^{\beta + 2\Delta_{1}} + G_{12} \epsilon^{\beta + 3\Delta_{1}}, \tag{8}$$

where  $G_7$  (estimated  $\rho_c$  reported here) and  $G_{10}$  -  $G_{12}$  are fitted constants. Critical temperatures and their estimated uncertainties obtained by Van Poolen *et al.* [1] are utilized.

The procedure is to simultaneously fit Eqs. (1), (2), (4), and (8) by the method of least squares. Eqs. (1) and (2) are only used to obtain the derivatives of  $\rho^{\ell}$  and  $\rho^{v}$ . These

derivatives are utilized in Eq. (7) along with  $\rho^{\ell}$  and  $\rho^{v}$  data to provide  $\rho_{x}$  data to be fitted by means of Eq. (8). The reported value of  $\rho_{c}$  is  $G_{7}$  from the intersection of  $\rho_{d}$  and  $\rho_{x}$  at the critical temperature.

To account for the effect of data choice on the estimate of  $\rho_c$ , data subsets are selected for each refrigerant. The six highest temperature data points are always included. Data sets then consist of points that start at randomly selected lowest values (assumed equally probable) and go serially through the six highest temperatures. Values of  $\rho^c$ ,  $\rho^v$ , T, and  $T_c$  are allowed to vary randomly about their mean values (the reported data) as normally distributed variables where the reported uncertainties are assumed three times the standard deviation. These reported experimental uncertainties are 0.5 kg/m³ for the coexisting densities and 0.1 K for the temperature.

The procedure is repeated between one and two hundred times within one computer run to achieve consistent results for the critical density, which is calculated as an average by,

$$\bar{\rho}_{c} = \frac{\sum_{i=1}^{n} \rho_{c,i}}{n} , \qquad (9)$$

where n is the number of times the procedure is repeated. Maximum absolute deviations between the data and the fitted equations are below 0.2 %. These differences are essentially random with little evidence of systematic trends.

The standard deviation of  $\rho_c$  is estimated by,

$$\sigma_{\rho_{c,n}} = \left[ \sum_{i=1}^{n} \frac{(\bar{\rho}_{c} - \rho_{c,i})^{2}}{n-1} \right]^{1/2}.$$
 (10)

This standard deviation takes into account the reported uncertainty in the data including the dependent variable (temperature and the critical value), deviations that arise from the selected functional form and its ability to fit the data, and the variations that might occur as different data subsets are tested. The reported value for the critical density is,

$$\rho_c = \bar{\rho}_c \pm 2\sigma_{\rho_c}. \tag{11}$$

The method is graphically illustrated (for R32) in Fig. 1.

# **APPLICATION TO R32**

The critical temperature used (Van Poolen *et al.* [1]) is  $351.33 \pm 0.28$  K (at  $2\sigma$ ). The procedure, applied to seven subsets of data between 338.24 and 348.61 K yields,  $\rho_c = 429.17 \pm 1.30$  kg/m³. Literature values (either from direct observation of meniscus behavior or use of a fitted, extrapolated straight line rectilinear diameter) are given and compared to our value in Table 1. Also see Fig. 1. Agreement is within published uncertainties for the majority of the references cited. Where there is disagreement, the upper limit of Schmidt and Moldover [6], 426 kg/m³, and of Kuwabara *et al.* [7] and Kuwabara *et al.* [8], 425 kg/m³, differ from our lower limit, 427.87 kg/m³, by 0.44 percent

and 0.67 percent, respectively.

## **APPLICATION TO R124**

The critical temperature used (Van Poolen *et al.* [1]) is  $395.35 \pm 0.36$  K (at  $2\sigma$ ). The procedure, applied to nine subsets of data between 375.27 and 390.65 K yields,  $\rho_c = 558.71 \pm 0.90$  kg/m³. Literature values (either from direct observation of meniscus behavior or use of a fitted, extrapolated straight line rectilinear diameter) are given and compared to our value in Table 2. Agreement is within published uncertainties.

#### **APPLICATION TO R152a**

The critical temperature used (Van Poolen *et al.* [1]) is  $386.30 \pm 0.24$  K (at  $2\sigma$ ). The procedure, applied to eight subsets of data between 372.35 and 383.71 K yields,  $\rho_c = 368.46 \pm 0.64$  kg/m³. Literature values (either from direct observation of meniscus behavior or use of a fitted, extrapolated straight line rectilinear diameter) are given and compared to our value in Table 3. Agreement is within published uncertainties.

#### **CONCLUSIONS**

A novel, intersection method is tested for R32, R124, and R152a which yields critical densities from experimental coexistence density data at temperatures where accurate measurements can be accomplished, that is, outside the very near critical region. This method utilizes the thermodynamic behavior of the liquid volume fraction in addition to that of the rectilinear diameter. Values obtained here (by the intersection method) for the critical density (with  $2\sigma$  uncertainties of about  $1.0 \text{ kg/m}^3$ ) agree with reported literature values with the exception of the two values mentioned above for R32.

#### **REFERENCES**

- [1] L.J. Van Poolen, C.D. Holcomb, and V.G. Niesen, V.G., 1996. "Critical temperature and density from liquid-vapor coexistence data: application to refrigerants R32, R124, and R152a," Fluid Phase Equilibria (in press, 1997).
- [2] C.D. Holcomb, V.G. Niesen, L.J. Van Poolen, and S.L. Outcalt, Fluid Phase Equilibria 91 (1993) 145-157.
- [3] V.G. Niesen, L.J. Van Poolen, S.L. Outcalt, and C.D. Holcomb, Fluid Phase Equilibria 97 (1994) 81-95.
- [4] S.B. Kiselev and J.V. Sengers, Int. J. Thermophys. 14 (1993) 1-32.
- [5] L.J. Van Poolen, Analysis of Liquid Volume and Liquid Mass Fractions at Coexistence for Pure fluids, NBSIR 80-1631, 1980.
- [6] J.W. Schmidt and M.R. Moldover, J. Chem. Eng. Data 39 (1994) 39-44.
- [7] S. Kuwabara, J. Tatoh, H. Sato, and K. Watanabe, "Critical parameters and vapor-liquid coexistence curve in the critical region for HFC-32", Thirteenth Japan Symposium on Thermophysical Properties, 1992, 69-72.
- [8] S. Kuwabara, S. Haruki, and K. Watanabe, High Temperatures-High Pressures, 26 (1994) 35-40.
- [9] P.F. Malbrunot, P.A. Meunier, G.M. Scatena, W.H. Mears, K.P. Murphy, and J.V. Sinka, J. chem. Eng. Data, 13 (1968) 16-21.
- [10] R.V. Singh, E.A.E. Lund, and I.R.Shankland, "Thermophysical properties of HFC-32," CFC and Halon International Conference, Baltimore, MD, 1991.

- [11] Y. Higashi, Int. J. Refrig., 17 (1994) 524-531.
- [12] Y. Higashi, H. Imaizumi, and S. Usuba, "Measurement of the critical parameters for HFC-32," Thirteenth Japan Symposium on Thermophysical Properties, 1992, 65-68.
- [13] M. Hirata, K. Nagahama, K. Saito, and N. Wakamatsu, Preprint of a paper presented at the 8th Autumn Meeting of the Soc. of Chem. Engrs. Japan, 1974, 444.
- [14] H. Kubota, Y. Tanaka, T. Makita, H. Kashiwagi, and M. Noguchi,, Int. J. Thermophys. 9 (1988) 85-101.
- [15] M. Fukushima and N. Watanabe, Trans. Of the JAR, 10 (1993) 75-86 (in Japanese).
- [16] I.R. Shankland, R.S. Basu, and D.P. Wilson, ASHRAE Trans. 96 part 2 (1990) 317-322.
- [17] L.J. Van Poolen, V.G. Niesen, C.D. Holcomb, and S.L. Outcalt, Fluid Phase Equilibria 97 (1994) 97-118.
- [18] W.H. Mears, R.F. Stahl, S.R. Orfeo, R.C. Shair, L.F. Kells, W. Thompson, and H. McCann, Ind. Eng. Chem. 47 (1955) 1449-1454.
- [19] Y. Higashi, M. Ashizawa, Y. Kabata, T. Majima, M. Uematsu, and K. Watanabe, JSME Int. J. 30 (1987) 1106-1112.
- [20] H.B. Chae, J.W. Schmidt, and M.R. Moldover, J. Phys. Chem. 94 (1990) 8840-8845.

## LIST OF SYMBOLS

 $\begin{array}{ll} G & \quad \text{parameter} \\ T & \quad \text{temperature} \end{array}$ 

X liquid volume fraction

## **Greek Letters**

 $\begin{array}{ll} \beta & & \text{scaling law exponent} \\ \Delta_1 & & \text{scaling law exponent} \end{array}$ 

ρ density

σ standard deviation

# **Subscripts**

1,2,...,12 denotes parameters critical point c d rectilinear diameter liquid volume fraction  $\ell \mathbf{v}$ literature values lit number of times the data selection - data fitting procedure is repeated n total density t density at the maxima in the liquid volume fraction  $\mathbf{X}$ 

# Superscripts

 $\begin{array}{ll} \ell & \quad \text{liquid} \\ v & \quad \text{vapor} \end{array}$ 

# FIGURE CAPTION

Fig. 1.  $\rho^{\ell}$ ,  $\rho_d$ ,  $\rho_x$ , and  $\rho^v$  versus temperature for R32

Comparison of  $\rho_{\rm c}$  (429.17  $\pm$  1.30 kg/m³) for R32 from this Study with Literature Values (Critical Temperatures given for Reference). Table 1.

T <sub>c, lit</sub> (K) (ITS-90)	351.33 - T <sub>c,lit</sub> (K)	$\rho_{c,lit} \\ (kg/m^3)$	$\frac{429.17 - \rho_{c,lit}}{\rho_{c,lit}} \times 100$ (%)	Source
$351.54 \pm 0.20$	-0.21	430	-0.19	(Malbrunot et al. $[9]$ ) <sup>2</sup>
$351.52 \pm 0.02$	-0.19	429.61	-0.10	(Singh <i>et al.</i> [10]) <sup>3</sup>
$351.26 \pm 0.01$	0.07	$428 \pm 5$	0.27	(Higashi [11]) <sup>3</sup>
$351.24 \pm 0.02$	0.09	$427 \pm 5$	0.51	(Higashi <i>et al.</i> [12]) <sup>3</sup>
$351.255 \pm 0.01$	0.09	$424 \pm 1$	1.22	$(Kuwabara et al. [7])^3$
$351.255 \pm 0.010$	0.075	$424\pm1$	1.22	(Kuwabara $et al. [8]$ ) <sup>3</sup>
$351.36 \pm 0.02$	-0.03	$419 \pm 7$	2.43	(Schmidt & Moldover [6]) <sup>2</sup>
		$428.50 \pm 1.83^{1}$	0.16	(Holcomb et al. $[2]$ ) <sup>2</sup>
$351.33 \pm 0.28$	0.00	$429.04 \pm 0.50$	0.03	(Van Poolen et al. $[1]$ ) <sup>2</sup>

 $<sup>^1</sup>$   $T_c$  used is 351.54 K from Malbrunot \textit{et al.}[9].  $^2$  Obtained  $\rho_c$  by extrapolation of a straight rectilinear diameter.  $^3$  Obtained  $\rho_c$  by direct observation of meniscus behavior.

Comparison of  $\rho_{\rm c}$  (558.71  $\pm$  0.90 kg/m³) for R124 from this Study with Literature Values (Critical Temperatures given for Reference). Table 2.

T <sub>c,lit</sub> (K) (ITS-90)	395.35-T <sub>c,lit</sub> (K)	$\rho_{c,lit} \\ (kg/m^3)$	558.71 - ρ <sub>c,lit</sub> 100 ρ <sub>c,lit</sub> (%)	x Source
$395.62 \pm 0.05$	-0.27	$560 \pm 2$	0.23	(Hirata <i>et al.</i> [13] & Kubota <i>et al.</i> [14]) <sup>2</sup>
$395.35 \pm 0.03$	0.00	$566 \pm 5$	-1.29	(Fukushima &Watanabe [15]) <sup>3</sup>
$395.36 \pm 0.15$	-0.01	$565 \pm 5$	-1.11	(Shankland <i>et al.</i> [16]) <sup>2</sup>
		$559.76 \pm 1.54^{1}$	0.19	(Van Poolen <i>et al.</i> $[17]$ ) <sup>2</sup>
$395.35 \pm 0.36$	0.00	$560.27 \pm 0.56$	0.28	(Van Poolen et al. [1]) <sup>2</sup>

 $<sup>^1</sup>$   $T_c$  used is 395.62 K from Hirata *et al.* [13].  $^2$  Obtained  $\rho_c$  by extrapolation of a straight rectilinear diameter.  $^3$  Obtained  $\rho_c$  by direct observation of meniscus behavior.

Table 3. Comparisons of  $\rho_c$  (368.46  $\pm$  0.64 kg/m³) for R152a from this Study with Literature Values (Critical Temperatures given for Reference).

T <sub>c, lit</sub> (K) (ITS-90)	386.30-T <sub>c,lit</sub> (K)	$\rho_{\rm c,lit} \\ (kg/m^3)$	$\frac{368.46 - \rho_{c,lit}}{\rho_{c,lit}} x 100$ (%)	Source
$386.62 \pm 0.5$	-0.32	$365 \pm 10$	0.95	(Mears <i>et al.</i> [18]) $^2$
$386.41 \pm 0.01$	-0.11	$368 \pm 2$	0.13	(Higashi <i>et al</i> . [19]) <sup>3</sup>
$386.32 \pm 0.10$	-0.02	369 ± 9	-0.15	(Chae <i>et al.</i> [20]) $^2$
		$368.81 \pm 0.96^{1}$	-0.09	(Holcomb et al. $[2]$ ) <sup>2</sup>
$386.30 \pm 0.24$	0.00	$368.89 \pm 0.38$	-0.12	(Van Poolen et al. $[1]$ ) <sup>2</sup>

 $<sup>^1</sup>$   $T_c$  used is 386.41 K from Higashi *et al.* [19]).  $^2$  Obtained  $\rho_c$  by extrapolation of a straight rectilinear diameter.  $^3$  Obtained  $\rho_c$  by direct observation of meniscus behavior.

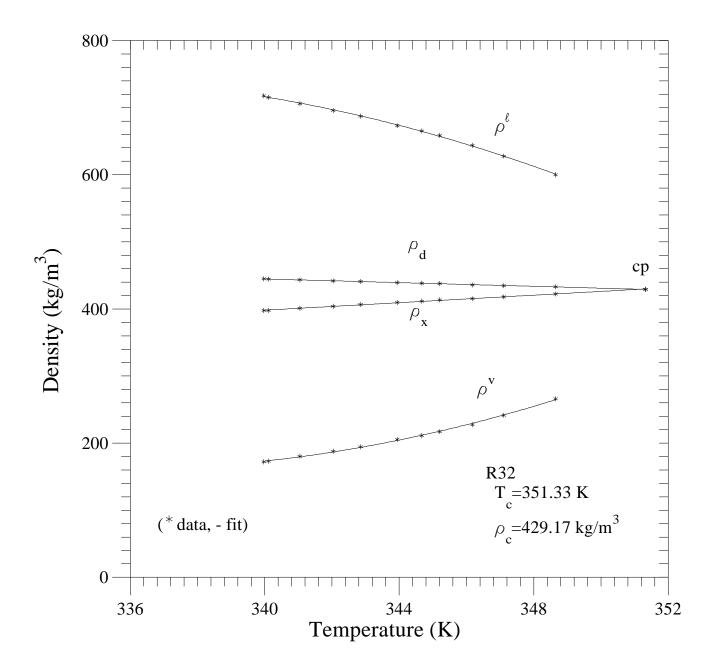


Figure 1